Méthodes multi-fluides eulériennes pour la description de brouillards de gouttes polydispersés qui s'évaporent

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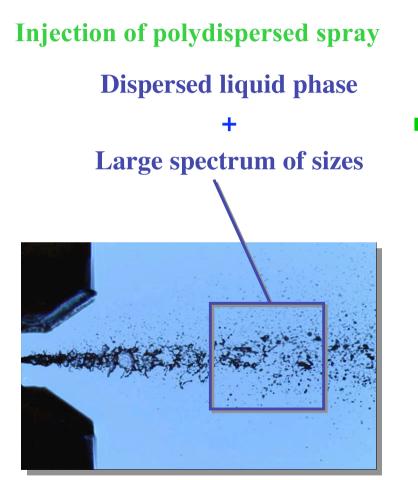


en collaboration avec J. Réveillon



Laboratoire CORIA CNRS - Université de Rouen

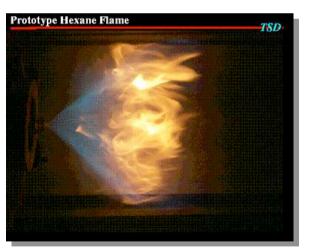




(Source C. Dumouchel, CORIA Rouen)

Spray flame

- Mass fraction of fuel in the gaseous phase
- Flame structure and dynamics
- Combustion efficiency
- Pollutants produced



(Source Prof. Edwards, Stanford)

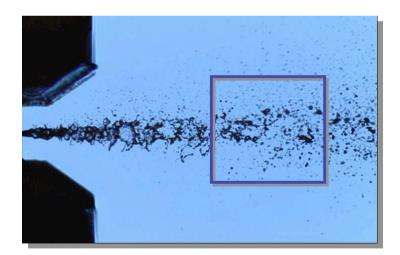
Modeling of the dispersed phase

Interactions droplets – gas

 → evaporation, drag, heat transfer

 Interactions between droplets

 → coalescence, breakup, ...





Key parameter : size

Modeling of the dispersed phase

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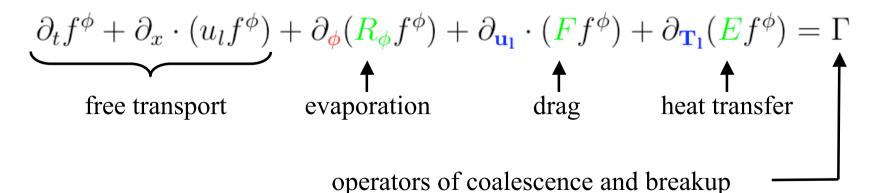
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Statistical model $f^{\phi}(t, x, \phi, \mathbf{u}_{\mathbf{l}}, \mathbf{T}_{\mathbf{l}})$: probability density of droplets

Transport equation of Boltzmann type (Williams 1958):



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Types of models developed for the spray simulation

∽ choice to satisfy key points for evaporating spray : polydispersion and correlations size/velocity

Multi-fluid model

 \hookrightarrow derivation of the method

Ejection of spray by vortices

→ comparisons between multi-fluid model and Lagrangian



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Lagrangian methods

" Stochastic Parcel Method " sampling of the probability density function O'Rourke 81, Duckowicz 80

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Advantages:

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Disadvantages:

- coupling: Eulerian description of the gas / Lagrangian description for the droplets
- cost for unstationnary problems

Lagrangian methods

" Stochastic Parcel Method " sampling of the probability density function O'Rourke 81, Duckowicz 80

Eulerian methods

Goal: give alternative discretization methods to largely used lagrangien ones

3 levels of modeling

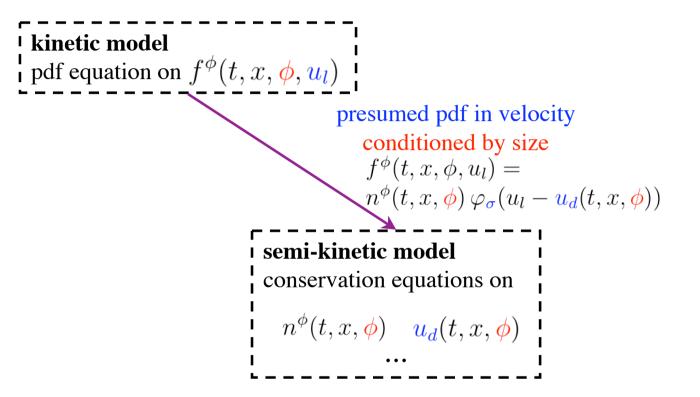
- distribution in size
- distribution in velocity
- correlations size/velocity

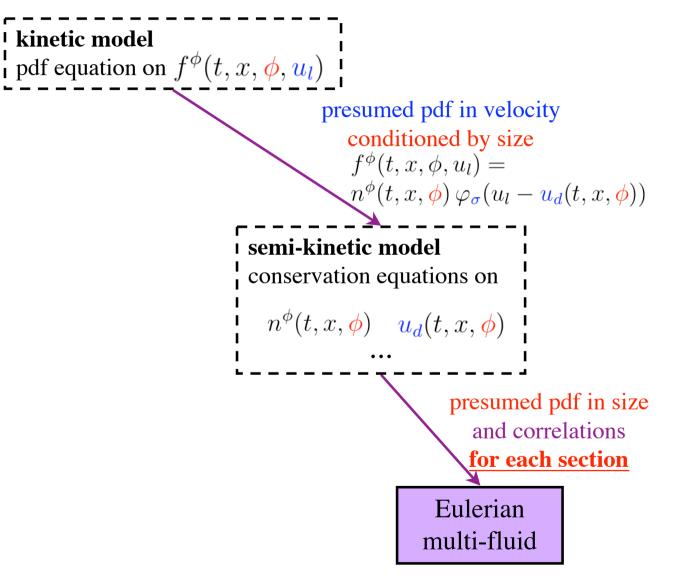
Objective : develop eulerian methods, with a cost as weak as possible, accurate for

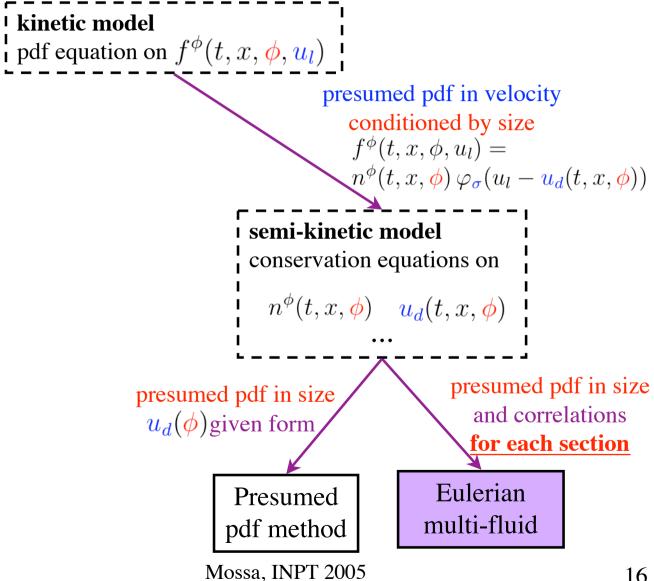
- the description of the **polydispersed** aspect
- **•** the description of the **dynamic** of the droplets
- the correlations size/velocity

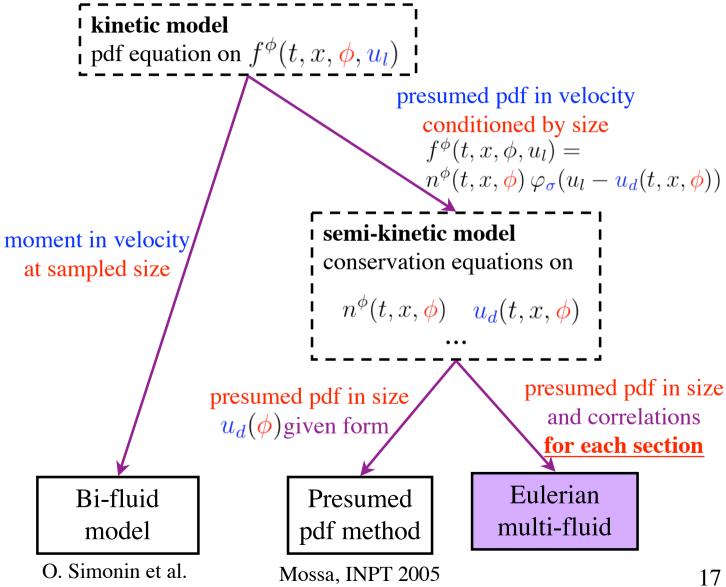
$$f^{\phi}(t, x, \phi, u_l)$$

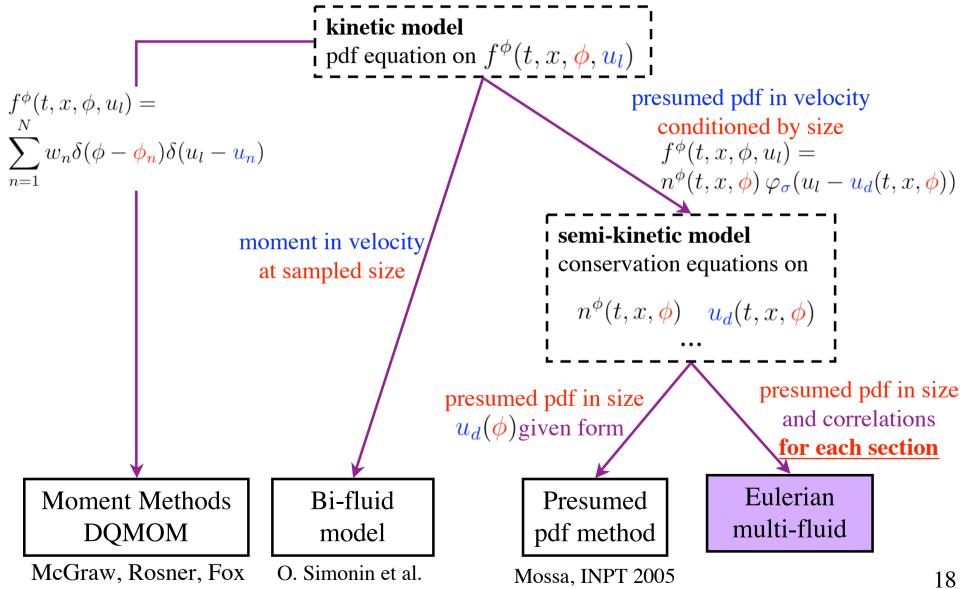
kinetic model pdf equation on $f^{\phi}(t, x, \phi, u_l)$













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Previous work

Eulerian multi-fluid model

Modeling

diluted laminar case

F. Laurent, M. Massot laminar case with coalescence or/and breakup F. Laurent, M. Massot, P. Villedieu + G. Dufour turbulent case J. Réveillon, M. Massot, C. Péra + R. Knikker

Numerical analysis of the evaporation and higher order methods
 F. Laurent / G. Dufour

Mathematic analysis : plane flames, multi-fluid models F. Laurent, M. Massot / G. Dufour, M. Massot

William's Transport Equation

 $f(t, x, S, u_l)$: probability density of droplets

Transport equation :

$$\partial_t f + \partial_x \cdot (u_l f) + \partial_S (R_s f) + \partial_{u_l} \cdot (F f) = 0$$

Stokes law for drag

$$F(S, u_{gaz}, u_l) = \frac{u_{gaz} - u_l}{\tau_p}$$

d² law for evaporation

$$R_s = \text{cste}$$

Semi-kinetic model: equations on

$$n(t, x, S) = \int f(t, x, S, u_l) du_l$$
$$u_d(t, x, S) = \frac{1}{n(t, x, S)} \int u_l f(t, x, S, u_l) du_l$$

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presumed pdf $f(t, x, S, u_l) = n(t, x, S)\delta(u_l - u_d(t, x, S))$

> Assumptions :

H1 Only one characteristic velocity at a given droplet size *H2* No dispersion of *f* at a given size for the velocity. \rightarrow laminar case

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$$\begin{cases} \partial_t n + \partial_x \cdot (n \, u_d) + \partial_\phi (n \, R_s) = 0\\ \partial_t (n \, u_d) + \partial_x \cdot (n \, u_d \otimes u_d) + \partial_\phi (n \, R_s \, u_d) = nF \end{cases}$$

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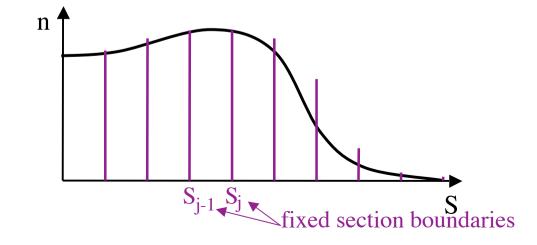
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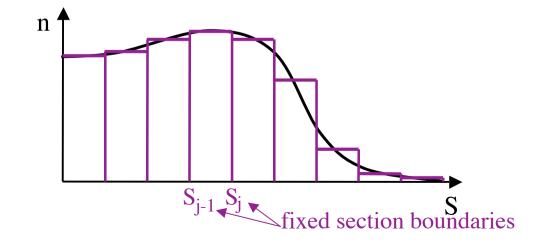
Multi-fluid model: finite volume discretization of n(t, x, S)

presumed profile of the distribution in each section



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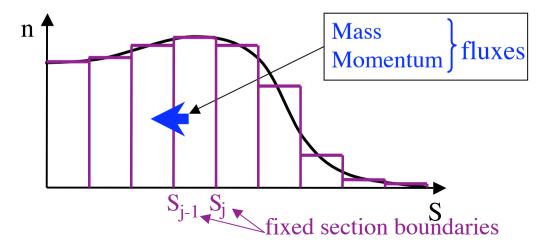


Multi-fluid model: finite volume discretization of n(t, x, S)

presumed profile of the distribution in each section

unknowns:
$$m_j(t,x) = \int_{S_{i-1}}^{S_i} \rho_l \frac{S^{3/2}}{6\sqrt{\pi}} n(t,x,S) dS$$
 $u_d^{(j)}(t,x)$

$$\begin{cases} \partial_t m^{(j)} + \partial_x \cdot (u_d^{(j)} m^{(j)}) = -(E_1^{(j)} + E_2^{(j)}) m^{(j)} + E_1^{(j+1)} m^{(j+1)} \\ \partial_t (m^{(j)} u_d^{(j)}) + \partial_x \cdot (m^{(j)} u_d^{(j)} \otimes u_d^{(j)}) = \\ -(E_1^{(j)} + E_2^{(j)}) m^{(j)} u_d^{(j)} + E_1^{(j+1)} m^{(j+1)} u_d^{(j+1)} + m^{(j)} F^{(j)} \end{cases}$$



Extensions the multi-fluid model

Scheme for the evaporation phenomenon

Classical multi-fluid method : 1st order method (F. Laurent M2AN 2006)

Extensions the multi-fluid model

Scheme for the evaporation phenomenon

- Classical multi-fluid method : 1st order method (F. Laurent M2AN 2006)
- Second order multi-fluid methods :
 - G. Dufour, P. Villedieu, M2AN 2006
 the profile of the distribution is exponential in each section

unknowns
$$n_j(t,x) = \int_{S_{j-1}}^{S_j} n(t,x,S) \, dS$$
, $m_j(t,x) = \int_{S_{i-1}}^{S_i} \rho_l \frac{S^{3/2}}{6\sqrt{\pi}} n(t,x,S) \, dS$

F. Laurent, M2AN 2006 the profile of the distribution is bi-affine in each section

unknowns
$$n_j(t,x) = \int_{S_{j-1}}^{S_j} n(t,x,S) \, dS$$
, $\widetilde{nS}_j(t,x) = \int_{S_{j-1}}^{S_j} S \, n(t,x,S) \, dS$

Numerical scheme

Transport part: pressureless gas

$$\begin{cases} \partial_t(\rho) + \partial_x \cdot (\rho u) &= 0\\ \partial_t(\rho u) + \partial_x \cdot (\rho u \otimes u) &= 0 \end{cases}$$

- Weakly hyperbolic system
 - \Rightarrow Development of delta-shocks
 - \Rightarrow Emergence of the vacuum state

Numerical scheme

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Transport scheme:

- Numerical approximations of pressureless gas
- → Finite volume kinetic scheme

Bouchut, Jin and Li, SIAM Numerical Analysis (2003)

- Scheme properties
 - Ability to treat delta shock and vacuum
 - Maximum principle on the velocity
 - Positivity of the density

Numerical scheme

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Splitting

- Separated treatment of transport, drag and evaporation
- → Strang splitting: Time 2nd order



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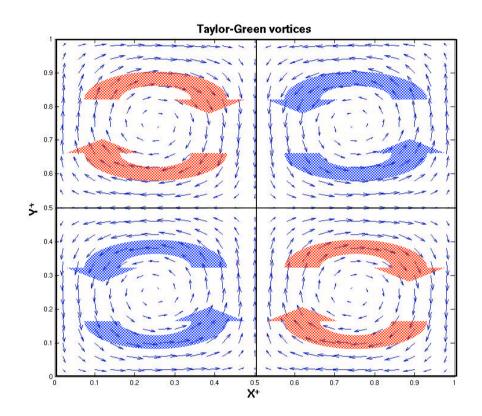
Multi-fluid model

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Ejection of spray by vortices

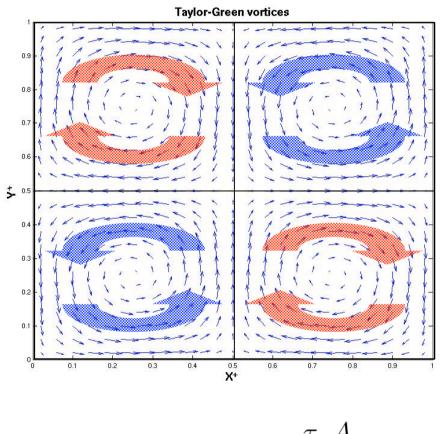
→ comparisons between multi-fluid model and Lagrangian

Gas configuration



- 2D Taylor-Green vortices • Euler stationary solution $\begin{cases}
 U_x(x,y) = A \sin(\frac{2\pi x}{\lambda})\cos(\frac{2\pi y}{\lambda}) \\
 U_y(x,y) = -A \cos(\frac{2\pi x}{\lambda})\sin(\frac{2\pi y}{\lambda})
 \end{cases}$
- One way steady simulation
- ⇒ Study of the dynamic of droplets ejection by vortices

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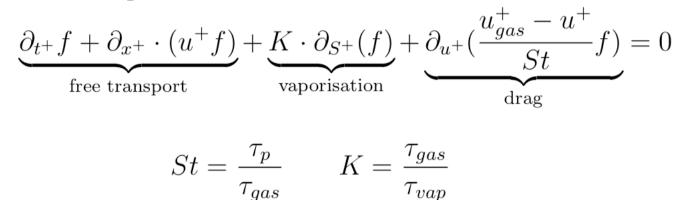


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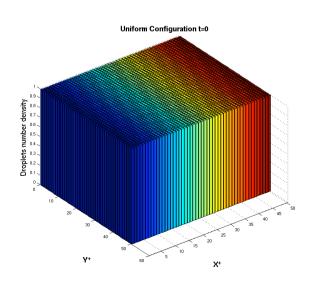
• Critical Stokes
$$St = \frac{\tau_p A}{\lambda} \longrightarrow St_c = \frac{1}{8\pi}$$

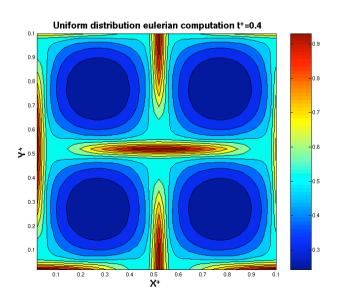
Droplet configuration

Non-dimensional equation



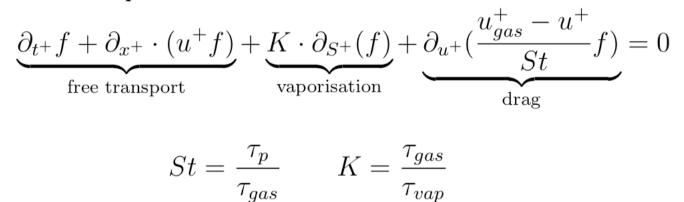
Uniform space distribution



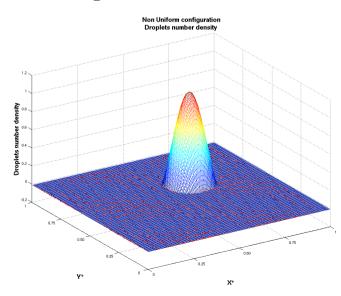


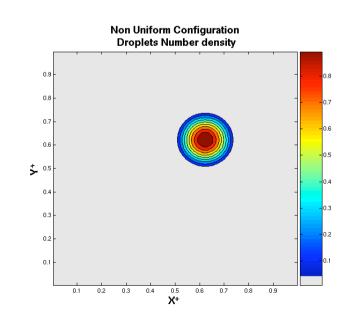
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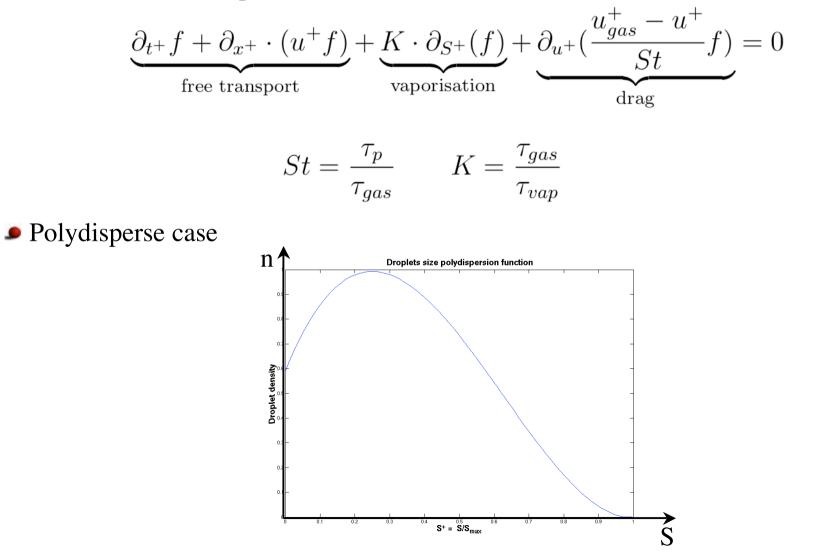
Non-uniform space distribution





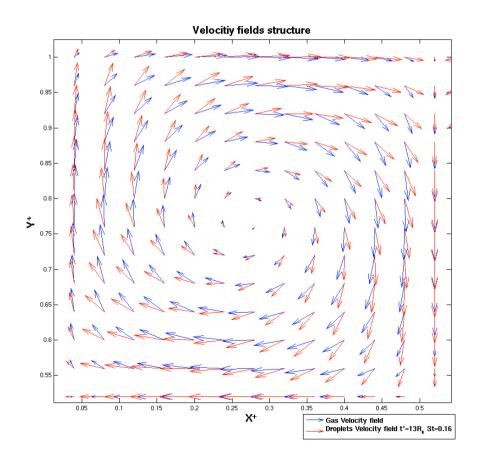
Droplet configuration

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Eulerian result analysis

- Toward a steady velocity structure for the droplets
 - \rightarrow Observed and proved in 1D sinus case
 - → Observed in our Taylor-Green configuration



Eulerian result analysis

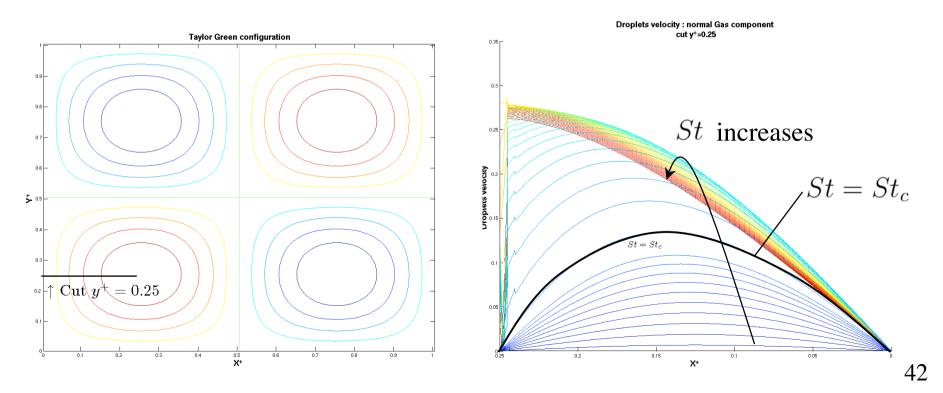
- Toward a steady velocity structure for the droplets
 - \rightarrow Observed and proved in 1D sinus case
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- Ejection from the vortices: characteristic time
 - Defined from the characteristic velocity of each droplet size
 - Allows characterization of the droplets dynamics

Eulerian result analysis

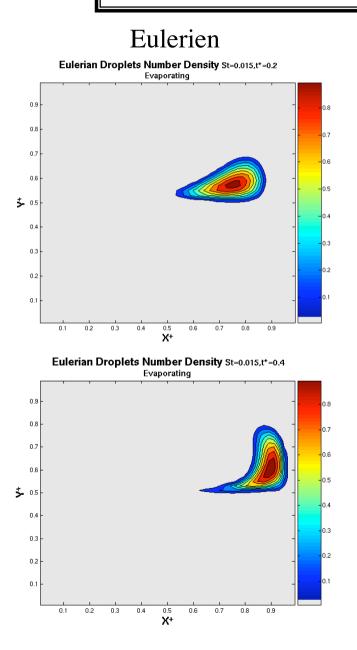
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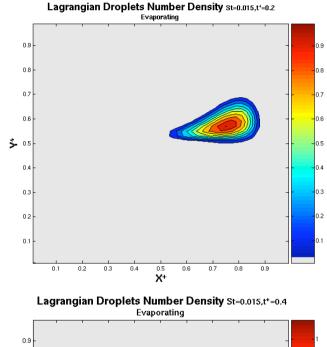
Ejection from the vortices: characteristic time

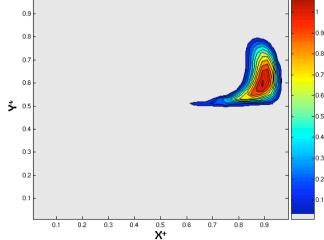


Eulerian Lagrangian comparison

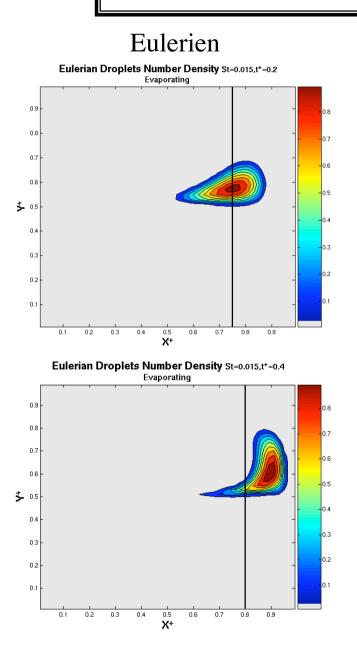


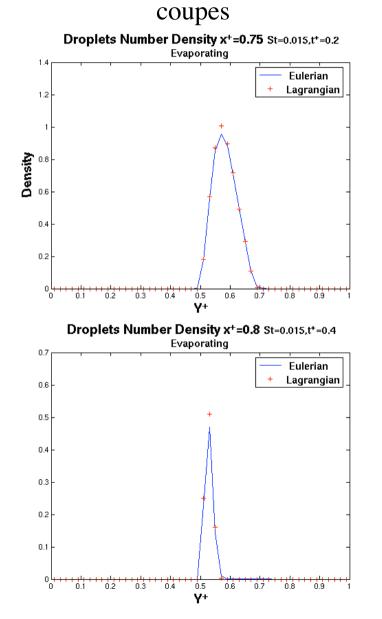
Lagrangien





Eulerian Lagrangian comparison

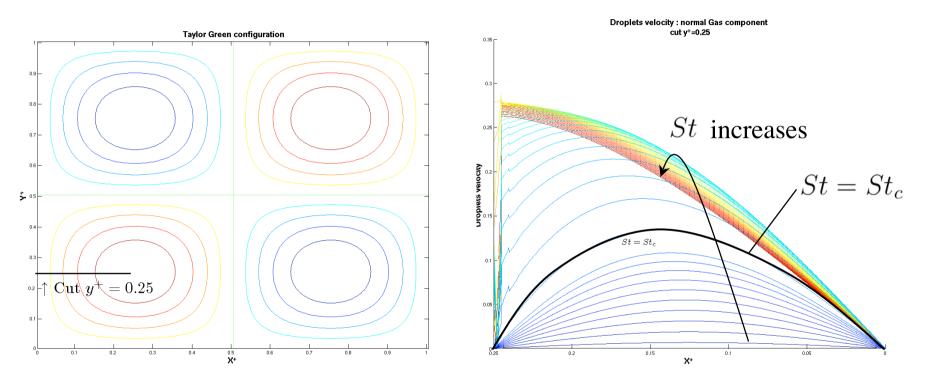




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Further results

• Case $St = 0.8 >> St_c$ Eulerian non-uniform simulation



Case St > St_c Lagrangian uniform simulation

Limit of the validity of the kinetic equation considered

 \Rightarrow consideration of particles interactions

Conclusion and Future work

Eulerian Multi-fluid method

- Derivation of a Eulerian method: validity domain
- Extension to higher order method for the evaporation phenomenon

Results on the studied configurations

- Interesting information extracted from the Eulerian simulation
- Encouraging Eulerian-Lagrangian comparisons results

Future work

- Going farther with the Taylor-Green configuration : analysis of the Eulerian results
- Addition of the collision phenomenon
- Working on new configurations: 2D-axis or 3D jet with turbulence

Comparison of the classical multi-fluid method with the higher order methods and the DQMOM method

Références principales

- <u>F. Laurent, M. Massot</u> Multi-fluid Modeling of Laminar Poly-dispersed Spray Flames : Origin, Assumptions and Comparison of the Sectional and Sampling Method CTM 2001
- <u>F. Laurent, M. Massot, P. Villedieu</u>, Eulerian multi-fluid modeling for the numerical simulation of coalescence in polydisperse dense liquid sprays JCP 2004
- <u>G. Dufour</u> Modélisation eulérienne des écoulements diphasiques à inclusions dispersées PhD Thesis, Université Paul Sabatier Toulouse 2005
- **G.** Dufour, P. Villedieu The sectional method revisited for evaporating sprays M2AN 2006
- <u>F. Laurent</u> Numerical analysis of eulerian multi-fluid models in the context of kinetic formulations for dilute evaporating sprays M2AN 2006
- <u>S. Jin, F. Bouchut, X. Li</u> Numerical approximations of pressureless and isothermal gas dynamics Siam J. Numer. Anal. 2003



Projet européen TIMECOP (2006-2007)

coordinateur de la tâche : F. Laurent, M. Massot

ACI Nouvelles Interfaces des Mathématiques, Ministère de la Recherche (2003-2006) coordinateurs : M. Massot, S. Descombes

ANR jeune équipe dynamique des sprays en évaporation et en combustion (2005-2008) coordinateur : M. Massot